1	Abiotic Reduction of 3-Nitro-1,2,4-triazol-5-one (NTO) and Other Munitions Constituents
2	by Wood-Derived Biochar through Its Rechargeable Electron Storage Capacity
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Abstract

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The environmental fate of 3-nitro-1,2,4-triazol-5-one (NTO) and other insensitive munitions constituents (MCs) is of significant concern due to their high water solubility and mobility relative to legacy MCs. Plant-based biochars have been shown to possess a considerable electron storage capacity (ESC), which enables them to undergo reversible electron transfer reactions. We hypothesized biochar can act as a rechargeable electron donor to effect abiotic reduction of MCs repeatedly through its ESC. To test this hypothesis, MC reduction experiments were performed using wood-derived biochars that were oxidized with dissolved oxygen or reduced with dithionite. Removal of aqueous NTO, an anion at circumneutral pH, by oxidized biochar was minimal and occurred through reversible adsorption. In contrast, NTO removal by reduced biochar was much more pronounced and occurred predominantly through reduction, with concomitant formation of 3-amino-1,2,4-triazol-5-one (ATO). Mass balance and electron recovery with ferricyanide further showed that (1) the amount of NTO reduced to ATO was relatively constant (85–100 μmol per gram of biochar) at pH 6–10; (2) the fraction of biochar ESC reactive toward NTO was ca. 30% of that toward ferricyanide; (3) the NTO-reactive fraction of the ESC was regenerable over multiple redox cycles. We also evaluated biochar transformation of other MCs, including nitroguanidine (NQ), 2,4-dinitroanisole (DNAN), and hexahydro-1,3,5-trinitro-1,3,5-triazine (RDX). While mass and electron balances could not be established due to sorption, DNAN and RDX reduction by reduced biochar was confirmed via detection of multiple reduction products. In contrast, NO was not reduced under any of the conditions tested. This study is the first demonstration of organic contaminant degradation through biochar's rechargeable ESC. Our results indicate biochar

is a regenerable electron storage medium and sorbent that can remove MCs from water through concurrent reduction and sorption, and is thus potentially useful for pollution control and remediation at military facilities.

Introduction

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Munitions constituents (MCs) used in explosive formulations have caused contamination of soil and groundwater at/near military sites across the U.S. ¹ 3-Nitro-1,2,4triazol-5-one (NTO), nitroguanidine (NQ), and 2,4-dinitroanisole (DNAN) are the major constituents in the insensitive formulation IMX-101, and NTO, DNAN, and hexahydro-1,3,5-trinitro-1,3,5-triazine (RDX) are the main constituents in the formulation IMX-104.² ³ While insensitive MCs are less prone to accidental detonation than legacy MCs such as 2,4,6-trinitrotoluene (TNT), they are more water-soluble. ⁴⁻⁶ For example, the solubility of NTO is 16,642 mg/L at 25 °C⁷, two orders of magnitude higher than that of TNT (100–128 mg/L at 25 °C).^{8,9} This suggests that insensitive MCs are more leachable and mobile in the environment and thus may pose a significant contamination problem and health concern.⁴, ¹⁰⁻¹⁴ Hence, it is necessary to develop cost-effective pollution control and remediation approaches for insensitive MCs at military sites. Biochar is a subset of black carbon produced through pyrolysis of biomass such as wood and grass. 15, 16 Because of its high specific surface area, biochar has been evaluated as a sorbent for removing organic chemicals ¹⁷⁻¹⁹ including pesticides, dyes, and MCs^{20, 21} such as TNT and RDX. However, the effectiveness of biochar as a sorbent has not been evaluated against insensitive MCs like NTO, which is an anion at circumneutral pH (pK_a = 3.76). $^{22-24}$ In addition to being a sorbent, biochar is capable of mediating redox reactions through two different mechanisms: electron conduction²⁵⁻²⁹ and electron storage.^{30, 31} The first mechanism requires external electron donor and acceptor to be in simultaneous contact with a conductive moiety in biochar, such as graphene domains^{32, 33} that conduct electrons from a donor to an acceptor such as 2,4-dinitrotoluene, RDX, and nitroglycerin. 26-29

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In contrast to the conduction mechanism, the electron storage mechanism involves redoxfacile functional groups in biochar. Electrons can be stored in biochar through reduction of its electron accepting functional groups, such as quinones, or removed from biochar through oxidation of its electron donating functional groups, such as hydroquinones. 30 The capacity of a biochar to store and reversibly exchange electrons with its surroundings is termed electron storage capacity (ESC), and is operationally defined to be the sum of electron donating capacity (EDC) and electron accepting capacity (EAC). 30, 31, 34 While EDC and EAC vary with the redox state of a biochar, the ESC is constant for a given pair of reductant and oxidant used to measure ESC.^{34, 35} Studies have shown that ESC is a common property of biochar prepared via pyrolysis of lignocellulosic biomass.³⁵ Biochar ESC can range from 0.2 to 7 mmol e⁻/g, is distributed over a broad range of reduction potential, and is highly reversible over multiple redox cycles. ^{30, 34, 36-39} Biochar can be an electron donor when its ESC is filled (i.e., its redox-facile functional groups reduced), and an electron accepter when its ESC is empty (i.e., its functional groups oxidized). Electrons stored in biochar have been shown to be partially available for abiotic reduction of metal(loid)s^{40, 41, 42} and for microbial reduction of nitrate.³¹ However, it is unknown whether electrons stored in biochar are available for organic contaminant degradation and, if so, to what extent, and whether this degradative capacity is regenerable. We hypothesized that biochar ESC can be accessed by MCs for reductive transformation, and that this process can be repeated through recharge of biochar ESC. This study was designed to (1) test this hypothesis, (2) determine the portion of ESC that is accessible to NTO and other MCs (DNAN, NQ, and RDX), and (3) produce data to support evaluation and development of biochar-based MC treatment/remediation systems. We performed batch experiments to assess the ability of wood-derived biochars to adsorb and degrade NTO in buffered solutions at pH 6–10

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and in artificial stormwater runoff (ASR) at pH 6. Parallel experiments were conducted using dithionite-reduced and air-oxidized biochars to study MC reduction and adsorption, respectively. **Materials and Methods** Chemicals. NTO and RDX were obtained from U.S. Army Armament Research Development and Engineering Center (Picatinny, NJ). The RDX contained 3.8% octahydro-1,3,5,7-tetranitro-1,3,5,7-tetrazocine (HMX) as an impurity. NQ (25% moisture content) and DNAN (98%) were purchased from Sigma-Aldrich (St. Louis, MO). 3-Amino-1,2,4-triazol-5one (ATO, >99%) was purchased from Princeton BioMolecular Research (Princeton, NJ). 2-Amino-4-nitroanisole (2ANAN) and 4-amino-2-nitroanisole (4ANAN) were purchased from Apollo Scientific (Cheshire, UK), and 2,4-diaminoanisole (DAAN, 99.6%) from Honeywell Fluka (Charlotte, NC). The three nitroso reduction intermediates of RDX, hexahydro-1-nitroso-3,5-dinitro-1,3,5-triazine (MNX), hexahydro-1,3-dinitroso-5-nitro-1,3,5-triazine (DNX), and hexahydro-1,3,5-trinitroso-1,3,5-triazine (TNX), were purchased from SRI International (Menlo Park, CA). Pure standards of NTO, NQ, DNAN, RDX, and HMX were acquired from AccuStandard (New Haven, CT). Additional chemicals for buffer solutions, ASR, pH control, high-performance liquid chromatograph (HPLC), and biochar redox titration, are provided in Table S1 of the Supporting Information. All chemicals were used as received. Biochars. Two wood-derived commercial biochars, Soil Reef biochar (SRB) and Rogue biochar (Rogue), were used. Physical-chemical properties of SRB and Rogue were measured and described in Section S1 (Supporting Information) and summarized in Table S2. SRB and Rogue are both derived from pine wood but were pyrolyzed at different temperatures (550 °C and 900 °C, respectively). SRB was chosen for this study because it has been field-tested for

stormwater treatment ⁴³ and its ESC and reversibility were well-characterized ^{31, 34, 40, 44} . Rogue				
was included because its BET surface area ($407\pm9~\text{m}^2/\text{g}$) and ESC ($7.07\pm0.15~\text{mmol/g}$) measured				
with titanium(III) citrate and dissolved O_2 (DO) were the highest of all commercial biochars we				
have tested. These values are roughly two times those of SRB ($158\pm3~\text{m}^2/\text{g}$ and 3.54 ± 0.13				
mmol/g, respectively).				
To facilitate MC reduction, SRB and Rogue particles in the 250–500 μm size range were				
ground at 4000 rpm for 3 min using a Beadbug 3 bead homogenizer (Benchmark Scientific Inc.,				
Sayreville, NJ) to obtain a particle size of $<53 \mu m$. Ground biochars were then oxidized with DO				
in continuously aerated deionized water to deplete stored electrons and bring the EDC of biochar				
to zero with respect to DO (E_{H} = +0.80 V vs. standard hydrogen electrode or SHE, at pH 7 and				
$P_{O_2} = 0.21$ atm). Based on our previous work, SRB and Rogue needed to be oxidized in aerated				
deionized water for at least 3 d to ensure thorough oxidation of reduced functional groups ^{34, 35} .				
Oxidized biochar samples were collected on a glass microfiber filter, dried at 65 °C for 24 h, and				
stored in a desiccator until use.				
For each biochar, two types of samples were prepared: DO-oxidized biochar (SRB _{OX} and				
Rogue _{OX}) and dithionite-reduced biochar (SRB _{RED} and Rogue _{RED}). SRB _{OX} or Rogue _{OX} were				
depleted of electrons and served as sorption controls, whereas SRB _{RED} or Rogue _{RED} were used to				
study MC reduction. To prepare dithionite-reduced biochars, SRB _{OX} and Rogue _{OX} were placed				
in an anaerobic glove box under 98±0.5% N_2 and 2.0±0.5% H_2 (P_{O_2} < 5 ppm) (Coy Laboratory,				
Grass Lake, MI) to deoxygenate. SRB _{OX} or Rogue _{OX} was then reduced with freshly prepared 25				
mM sodium dithionite in 100 mM citrate buffer at pH 6.4 for 3 d (measured $E_{H} = -0.43 \ V \ vs.$				
SHE). Dithionite was added in excess and was replenished as needed. After reduction, SRB _{RED}				
and Roguered were collected on a glass microfiber filter, rinsed thoroughly with copious DO-				

140 free deionized water, vacuum-dried, and stored in a desiccator in a glove box until use. All 141 reported data are based on dry mass. 142 Batch experiments. Batch reactors were set up and experiments were conducted inside an 143 anaerobic glove box. SRB_{RED} or Rogue_{RED} was used for MC reduction experiments, and SRB_{OX} 144 or Rogue_{OX} was used as nonreactive control and for MC sorption experiments. A summary of the 145 conditions for batch experiments, including the initial concentration of MC, biochar dose, and 146 solution matrices, is provided in Table S3. 147 NTO reduction in buffer solutions. Batch experiments were performed with SRB for NTO 148 reduction in pH 6, 8 and 10 buffer solutions. To initiate an experiment, a predetermined amount 149 of SRB_{OX} or SRB_{RED} (0.40 or 0.80 g/L) was added to amber borosilicate reactors containing 125 150 mL of 110 µM NTO in 50 mM pH buffer. MES, Tris, and CAPSO were used to maintain the pH 151 at 6.0±0.1, 8.0±0.1, and 10.0±0.1, respectively. Blanks (no biochar) were prepared identically. 152 All reactors were placed on an orbital shaker at 100 rpm. Samples of 0.625 mL were taken at 153 different elapsed times and immediately passed through 0.22-um PTFE syringe filters for HPLC 154 analysis. Experiments were performed for up to 600 h until the concentration of ATO plateaued. 155 All collected samples combined accounted for <10% of the total solution volume in each reactor. 156 Removal of NTO and ATO due to sampling was accounted for to establish mass balance. After 157 reaction, SRB was retrieved on a glass microfiber filter, vacuum-filtered, and rinsed thoroughly 158 with deionized water. Since NTO and ATO ($pK_a = 8.71$, Figure S1) did not sorb to SRB at pH 10 159 (Figures 1(c) and S2), SRB samples retrieved from pH 6 and 8 reactors were extracted with 50 160 mL of 50 mM CAPSO solution at pH 10 to recover sorbed NTO and ATO. Extraction was 161 performed for up to 600 h and extracts (0.625 mL) were sampled at different times for HPLC 162 analysis.

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SRB electron content measurement. The electron content (i.e., EDC) of fresh SRB_{RED} and spent SRB_{RED} recovered from NTO experiment was measured using ferricyanide as an oxidant $(E_H = +0.43 \text{ V vs. SHE})^{45}$. Reactors containing fresh SRB_{OX} and SRB_{OX} exposed to the same NTO solution were included as controls. SRB samples were placed in 0.23 L of 1 mM ferricyanide solution in 50 mM MES, Tris, or CAPSO buffer. Electrons transferred from SRB to ferricyanide were determined based on the amount of ferricyanide consumed. Concentration of ferricyanide was measured by absorbance at 420 nm, using a Vernier LabQuest 2 UV-vis spectrophotometer (Beaverton, OR). The extinction coefficients of ferricyanide at pH 6, 8, and 10 were 1135 ± 40 , 1152 ± 40 , and $1058 \pm 40 \text{ M}^{-1} \cdot \text{cm}^{-1}$, respectively. Each SRB sample was oxidized with ferricyanide for up to 72 h. After EDC measurement, SRB was collected by filtration and vacuum-dried at 65 °C for weight measurement. ESC reversibility for NTO reduction. Additional experiments were performed to assess the reversibility of ESC with respect to NTO reduction over three redox cycles. To prevent sorption of NTO and ATO to SRB, experiments were run at pH 10 in 50 mM CAPSO buffer. Four pairs of duplicate reactors containing 125 mL of 100 µM NTO were prepared: 0.80 g/L of SRB_{RED} was added to the first two pairs of reactors, 0.80 g/L of SRB_{OX} was added to the third pair of reactors, and no biochar was added to the last pair of reactors. For each cycle, NTO reduction was run for 24 h following the same procedures as described above. After reaction, SRB was retrieved on a glass microfiber filter, vacuum-filtered, thoroughly rinsed with 50 mL of 50 mM CAPSO buffer three times. For the first pair of reactors containing SRB_{RED}, the retrieved SRB_{RED} was reduced with 50 mL of 1 mM dithionite (total e⁻ content = 100 µmol) for 24 h, washed with 50 mL of deoxygenated deionized water three times, and used in the next cycle of NTO reduction. This pair of reactors was labeled as "ESC-recharged". Note that, based on SRB

porosity, any residual dithionite remaining in the pores of SRB_{RED} would contribute to <1% of
the electrons transferred to NTO. For the second pair of reactors containing SRB_{RED} , the
retrieved SRB _{RED} was labeled "ESC-not-recharged". The procedures for the second cycle of
NTO reduction were the same, where both "ESC-recharged" and "ESC-not-recharged" SRB_{RED}
were added to 125 mL of 100 μM NTO in 50 mM CAPSO buffer and allowed to react for 24 h.
After the second cycle, "ESC-recharged" SRB _{RED} was reduced again with dithionite for the third
cycle. Biochar-free and SRB_{OX} controls were included in each cycle.
MC reduction in ASR. To assess the performance of biochar in synthetic stormwater, batch
experiments were also carried out in ASR, which was established based on the composition of
stormwater samples collected from an east coast U.S. Navy facility and consisted of 0.38 mM
Na^{+} , 0.24 mM K^{+} , 0.09 mM NH_{4}^{+} , 0.08 mM Ca^{2+} , 0.05 mM Mg^{2+} , 0.65 mM Cl^{-} , 0.15 mM SO_{4}^{2-}
and 0.02 mM NO ₃ ⁻ . ⁴⁶ Batch experiments were performed with Rogue _{OX} or Rogue _{RED} for NTO,
NQ, DNAN, and RDX in ASR at pH 6. To compare SRB and Rogue, an additional experiment
with SRB (SRB $_{\text{OX}}$ or SRB $_{\text{RED}}$) was run for NTO in ASR at pH 6 under identical conditions. The
pH was controlled at 6.0±0.2 during experiment using 0.05 N HCl. The solution was sampled
(0.625 mL for NTO and DNAN, 6 mL for RDX) at different times. A portion of the RDX sample
(5 mL) was used for NO_2^- analysis and the rest for RDX and transformation product
measurement. After each experiment, biochar samples were subjected to solvent extraction.
NTO, NQ, and daughter products were extracted with a 3:7 (v/v) mixture of acetonitrile and
0.1% trifluoroacetic acid, whereas DNAN, RDX, and daughter products were extracted with an
8:2 mixture of acetonitrile and 0.1% trifluoroacetic acid. ⁴⁷ Each biochar sample was extracted
three times. Samples of MCs and daughter products from multiple extractions were combined to
obtain the total recovery.

MC sorption isotherm. Experiments were performed to obtain MC sorption isotherms for Rogue_{OX} in ASR at pH 6. To obtain an isotherm, a series of duplicate amber borosilicate reactors were set up that contained ASR and an MC at different initial concentrations. The biochar doses and MC concentration ranges (Table S4) were selected based on preliminary experiments and the solubility of each MC used. Samples (0.8 mL) were collected at different incubation times and passed through 0.2-μm PTFE syringe filters for HPLC analysis. Experiments were run for up to 400 h until an apparent sorption equilibrium was reached (variations in aqueous concentrations <1% per hour). pH was maintained at 6.0±0.2 using 0.05 N HCl. For comparison, we ran an additional set of batch experiments to obtain the sorption isotherm for NQ and SRB_{OX} in 50 mM Tris buffer at pH 8.0±0.1.

For each MC, the mass sorbed per gram of biochar (C_s) was plotted against the equilibrium aqueous concentration (C_{eq}) , and the data were fitted to a Langmuir isotherm (Eq. 1) using the least-square method.

$$C_s = \frac{K_L C_{eq} C_{s,max}}{1 + K_L C_{eq}}$$
 [Eq. 1]

where C_s (µmol/g) is sorbed MC mass per gram of biochar, C_{eq} is equilibrium MC concentration in water (µM), $C_{s,max}$ (µmol/g) and K_L (µM⁻¹) are fitted maximum sorption capacity and sorption affinity, respectively. After each sorption experiment, biochar samples that sorbed the maximum mass of MC were subjected to solvent extractions, as described above for MC reduction experiments.

Analytical methods. MCs were analyzed using an Agilent 1200 Series HPLC (Santa Clara, CA) equipped with an Agilent 1260 diode array detector. The hydrophilic analytes NTO, ATO, and NQ were separated using a Thermo Scientific (Waltham, MA) Hypercarb porous graphitic carbon column (4.6 mm×100 mm, 5 μm particle size). A mixture of acetonitrile and 0.1%

trifluoroacetic acid was used as eluent at a flow rate of 2.0 mL/min. The run time was 10 min and the temperature was 34.0 °C. NTO, ATO, and NQ were detected at 7.9, 4.3, and 5.8 min and quantified based on absorbance at 318, 210, and 260 nm, respectively. The hydrophobic analytes, including DNAN, RDX, HMX, and their daughter products, were separated using an Agilent Zorbax SB-C18 column (4.6 mm×50 mm, 3.5 µm particle size). A mixture of phosphate buffer and methanol was used as eluent at a flow rate of 1.7 mL/min. The run time was 7 min and the temperature was ambient. DNAN and RDX were detected at 4.8 and 3.4 min, respectively, and quantified based on absorbance at 214 nm. The same method was used to quantify daughter products of DNAN⁴⁸ and RDX^{49,50}: 2-ANAN, 4-ANAN, and DAAN were measured at 4.2 min (254 nm), 3.2 min (234 nm) and 2.3 min (210 nm), respectively, and MNX, DNX, and TNX were detected at 2.9, 2.4, and 1.9 min, respectively, based on absorbance at 234 nm. Nitrite, a potential RDX reduction product, ⁵¹ was measured using Hach NitriVer® 3 Nitrite Reagent (Loveland, CO) and a Vernier LabQuest 2 UV-vis spectrophotometer.

Results and Discussion

NTO removal by SRB. Figure 1 shows NTO removal by SRB_{OX} and SRB_{RED} at pH 6, 8, and 10 and the mass balance at the end of each experiment. SRB_{OX} adsorbed NTO in small amounts which were largely recovered by extraction. NTO sorption decreased with increasing pH, with 80%, 93% and 99% of the initial mass remaining in solution at equilibrium at pH 6, 8, and 10, respectively (solid blue bars in Figure 1(d)). As NTO is anionic (pK_a 3.76)²² at all three pH values, the decreasing sorption (24, 10, and 2 μmol/g, respectively) was most likely due to increasingly negative surface charge of SRB with pH.⁵² Extraction of SRB_{OX} from pH 6 and 8 reactors with CAPSO buffer yielded mass balances of 94% and 101%, respectively.

In contrast, significantly more NTO was removed from solution by SRB_{RED}, and ATO was produced concomitantly, indicating NTO was reduced to ATO by SRB_{RED}, as shown in Eq. 2. Reduction of NTO to ATO was rapid in the first 24 h and continued at decreasing rates for up to 600 h. Note that Figure 1(a)–(c) are semi-log plots and therefore the changing slopes represent decreasing pseudo-first-order rate constants. The decreasing NTO reduction rate constants could be due to one of two reasons (or both). First, it has been shown that a large portion of the ESC resides in the interior of SRB particles,³⁴ and the rate of access is limited by pore diffusion, which is approximately two orders of magnitude slower than diffusion in the bulk solution. Second, the redox-active functional groups (or ESC) of biochar are distributed over a range of reduction potentials^{34, 53} and hence would react with NTO at a spectrum of rate constants. The decreasing NTO reduction rate over time likely reflects a combination of slow diffusion through tortuous channels to access reactive ESC residing in deep pores in biochar interior, and slow reaction with functional groups of increasing reduction potentials (i.e., decreasing reactivities).

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$$N-NH + 7H^{+} + 6e^{-} \rightarrow N-NH$$
 (3.76

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$$N-NH + 6H^{+} + 6e^{-} \rightarrow N-NH$$
 (pH>8.71) [Eq. 2]

The combined aqueous NTO and ATO masses were about 80% at pH 6 and 8 and virtually 100% at pH 10. This suggests that, in contrast to NTO, ATO was sorbed to a similar extent at pH 6 and 8 but negligibly at pH 10. This was independently confirmed, as shown in Figure S2. As the pK_a of ATO had not been reported, we performed a titration (Section S2) and determined the pK_a of ATO to be 8.71 (Figure S1). This is in agreement with the pH effect on ATO sorption, as ATO would be predominantly neutral at pH 6 and 8 and negatively charged at pH 10, where

sorption would be hindered by electrostatic repulsion between negatively charged ATO and biochar surface (pH_{zpc} = $2-3^{52}$).

Because complete mass balance was achieved at pH 10 based on aqueous NTO and ATO (dotted line in Figure 1(c)), all NTO removal by SRB_{RED} was attributed to reduction. This also confirms that no alkaline hydrolysis of NTO or ATO occurred at pH 10 over 600 h. Following extraction, the mass balances for all SRB_{RED} reactors were between 91% and 100% (Figure 1(d)). The remaining sorbed mass was likely sorbed through interactions that could not be reversed by pH increase, such as the π - π donor-acceptor interactions²¹ between graphitic regions of SRB and the aromatic NTO⁻ anion²³.



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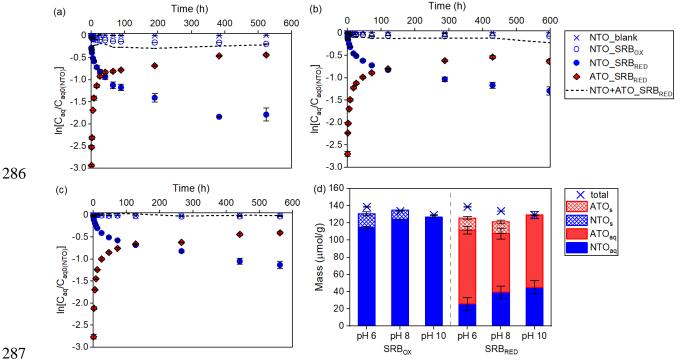


Figure 1. Aqueous concentration (C_{aq}) of NTO and ATO over time with 0.80 g/L of SRB_{OX} or SRB_{RED} at (a) pH 6 (50 mM MES) (b) pH 8 (50 mM Tris), and (c) pH 10 (50 mM CAPSO), and (d) mass balance at the end of experiment. The Y axis in panels (a)–(c) shows the natural

logarithm of C_{aq} of NTO or ATO relative to the initial NTO concentration ($C_{aq0(NTO)}$ =110 μM).
The total mass is based on blank (without SRB). NTO_{aq} and ATO_{aq} are the final masses in the
aqueous phase, and NTOs and ATOs the sorbed masses extracted from solid.
ESC available for NTO reduction. Figure 2(a and b) shows aqueous NTO removal and ATO
formation with 0, 0.40, and 0.80 g/L of SRB_{OX} or SRB_{RED} at pH 10. NTO removal and ATO
formation were observed with SRB_{RED} , but not SRB_{OX} . When the SRB_{RED} mass increased from
0.40 to 0.80 g/L, the amounts of NTO removed and ATO produced both doubled (Figure 2(c)),
indicating the quantity of electrons per gram of SRB _{RED} available for NTO reduction within 600
h, that is, the fraction of SRB's ESC that was accessible to and of sufficiently low reduction
potential to reduce NTO, was constant. Given the fact that 6 electrons per molecule are required
to convert NTO to ATO (Eq. 2), the portion of ESC that was available for NTO reduction at pH
10 was 499 and 503 $\mu mol\ e^-\!/g$ SRB, respectively, based on the amounts of NTO reduced
$(83.2\pm0.8~\mu mol/g)$ and ATO formed $(83.9\pm1.6~\mu mol/g).$ At pH 6 and 8, the total amounts of
ATO formed with 0.80 g/L of SRB_{RED} were 100 ± 7 and 82 ± 8 μ mol/g (Table S5), corresponding
to 600 and 492 μmol e ⁻ /g, respectively, as shown in Figure 3 (red bars).

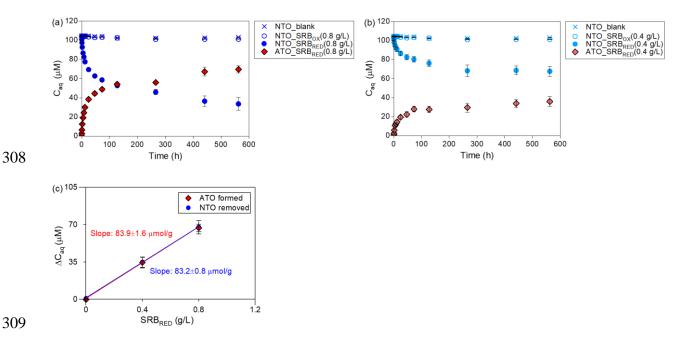


Figure 2. (a) Aqueous concentration (C_{aq}) of NTO and ATO over time with 0.80 g/L of SRB_{OX} or SRB_{RED} at pH 10. (b) C_{aq} of NTO and ATO over time with 0.40 g/L of SRB_{OX} or SRB_{RED} at pH 10. (c) Concentrations of ATO produced and NTO removed by SRB_{RED}.

Although the reduction potential distribution of biochar's ESC has not been fully delineated, it appears to cover a broad range of potential. Because one gram of SRB_{OX} can store up to 4.0 mmol of e^- with dithionite as a reductant ($E_H = -0.43 \text{ V}$ vs. SHE at pH 6.4), 4, 54 the result above suggests that only 500–600 μ mol/g of the stored electrons in SRB_{RED}, or 12–15% of SRB's ESC, had sufficiently low reduction potential to reduce NTO. An effort to establish an electron balance for NTO reduction by SRB_{RED} using DO as an oxidizing agent ($E_H = +0.80 \text{ V}$ vs. SHE at pH 7) was hindered by the volatile nature of DO. Therefore, ferricyanide ($E_H = +0.43 \text{ V}$ vs. SHE at pH 7) was used instead to retrieve electrons from SRB_{RED} before and after reaction with NTO. 55 If all the electrons accessible to and reactive toward NTO could also reduce ferricyanide, the amount of electrons remaining in used SRB_{RED} at the end of an NTO reduction experiment

324	would be the difference between all retrievable electrons from unused fresh SRB _{RED} and the				
325	electrons consumed by NTO:				
326	e ⁻ retrieved from NTO-exposed SRB _{RED}				
327	= (e ⁻ retrieved from fresh SRB _{RED}) – (e ⁻ consumed for NTO reduction) [Eq.3]				
328	The data in Figure 3 confirm this relationship and show the ESC of SRB that is reactive				
329	towards NTO was 26-38% of that reactive towards ferricyanide, suggesting NTO is significantly				
330	more difficult to reduce than ferricyanide.				
331	The ESC retrieved by ferricyanide increased notably from 1591 $\mu mol/g$ to 1899 $\mu mol/g$				
332	when pH increased from 6 to 8. Since the reduction potential of ferricyanide is pH-independent,				
333	this result suggests that the functional groups that constitute ESC have acid-base properties and				
334	deprotonate between pH 6 and 8. To illustrate this pH effect, we use 9,10-anthrahydroquinone-				
335	2,6-disulfonate (AH ₂ QDS, $pK_a = 7.6$) as a hypothetical hydroquinone in SRB to show (Section				
336	S4 and Figure S3) that the thermodynamic driving force for the oxidation of AH ₂ QDS by				
337	ferricyanide is lower at pH 6 (when the hydroquinone is fully protonated) than at pH 8 and 10				
338	(when the hydroquinone is singly deprotonated). Hence, biochar's ESC is a function of pH, even				
339	when measured using the same reductant and oxidant (e.g., dithionite and ferricyanide), and pH				
340	should be specified when ESC is reported.				

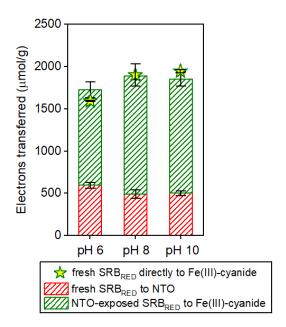


Figure 3. Electron balance for NTO reduction by SRB_{RED} . Electrons of fresh SRB_{RED} consumed by NTO was calculated based on ATO formation.

Rechargeability of ESC for NTO reduction. The ESC of biochar has been shown to be reversible over multiple oxidation-reduction cycles.^{34, 35} This suggests that, as a rechargeable electron storage medium, biochar should be able to reduce contaminants repeatedly through recharging. This is demonstrated in Figure 4. Consistent with our earlier results, removal of aqueous NTO by SRB_{OX} was negligible at pH 10 (which was chosen to minimize sorption of NTO and ATO). In contrast, NTO was transformed to ATO stoichiometrically by SRB_{RED}. For the first 24-h cycle, the NTO removed from solution by SRB_{RED} was *ca.* 32 μM (corresponding to *ca.* 38 μmol/g SRB_{RED}, Figure S4), in good agreement with the data in Figure 1(c). The used SRB_{RED} ("ESC-not-recharged") recovered from the first cycle was unable to reduce NTO to any measurable extent upon transfer to a fresh NTO solution, suggesting the most reactive electrons had been exhausted. When the used SRB_{RED} was recharged with dithionite ("ESC-recharged"), NTO was reduced to ATO in comparable quantities to those in the first cycle (Figure S4). Stoichiometric

conversion of NTO to ATO was also observed in the third cycle, albeit in a slightly lower
quantity (32 μ mol/g). This indicates the fraction of the ESC that had sufficiently low redox
potentials (and thus sufficiently high reactivity) to reduce NTO could be recharged repeatedly.
The electrons in the ESC that could reduce NTO within 24 h in the second and third cycles were
101% and 85% that in the first cycle, respectively, demonstrating high reversibility of the ESC of
SRB for NTO transformation. Therefore, if placed in a sufficiently reducing environment, such
as a stormwater treatment or groundwater (bio)remediation system, biochar may be repeatedly
recharged, either chemically ³⁴ or microbially ^{31,43} , and continuously degrade contaminants such
as NTO and other munitions compounds (shown below).
Much research to date on the fate and treatment of NTO has focused on sorption ⁵⁶⁻⁵⁸ and
biodegradation. ⁵⁹⁻⁶¹ Because ATO can be readily mineralized to innocuous products such as CO ₂
NH_4^+ , and N_2 , 62 reduction to ATO may be a first step to achieve complete NTO mineralization.
Recent studies further showed that NTO can be abiotically reduced to ATO by geo-constituents
including the hematite-Fe ²⁺ redox couple ²⁴ , FeS minerals ⁶³ , hydroquinones and humic acids ⁶⁴ .
Because ESC is a universal property of plant-based biochars, ³⁵ our results suggest that pyrogenic
carbon, another redox-active geo-constituent that is ubiquitous in soils and sediments, 65, 66 may
also mediate the abiotic reduction of NTO through the same mechanism. Our result therefore has
broader implications for the roles of black carbon in controlling the fate of MCs in subsurface
environments as well as in engineered systems.

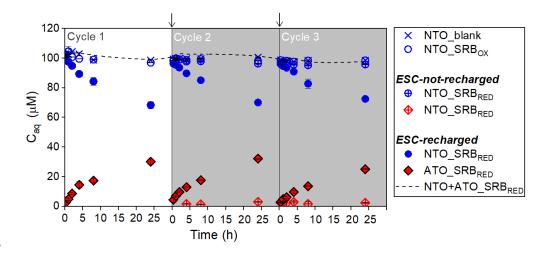


Figure 4. Rechargeability of biochar ESC for repeated NTO reduction. Aqueous concentrations (C_{aq}) of NTO and ATO are shown as a function of time with 0.80 g/L of SRB_{OX} or SRB_{RED} at pH 10. After each cycle, NTO solution was replaced and, for "ESC-recharged", the recovered SRB_{RED} was recharged with dithionite for the next reaction cycle (\downarrow). The error bars for the SRB_{RED} data in the first cycle represent one standard deviation from four replicates.

MC sorption by biochar. A goal of this study was to evaluate the potential utility of biochar for removing MCs in treatment systems. To that end, we evaluated removal of NTO, NQ, DNAN, and RDX by biochar through two mechanisms, i.e., sorption and abiotic reduction. Unlike NTO, which is negatively charged under circumneutral conditions, NQ, DNAN, and RDX are neutral and less water-soluble, which suggests that sorption may play a greater role in their removal by biochar. Hence, we first characterized the sorption of these MCs to biochar before investigating their potential reductive transformation. Rogue, a commercial wood-derived biochar with high BET surface area and ESC, was used to assess its sorption and reduction capacities for MCs in ASR at pH 6. As shown in Figure S5, all four MCs were removed rapidly from solution as soon

as oxidized Rogue (Rogue_{OX}) was added. Removal subsequently slowed but continued for up to 340 h until an apparent equilibrium was reached.

The equilibrium concentration of sorbed and aqueous MCs from Figure S5 were used to construct sorption isotherms. The data for each MC were fitted to a Langmuir isotherm, as shown in Figure 5 and Table 1. The maximum sorption capacities (C_{s, max}) of Rogue for NTO, NQ, DNAN, and RDX were 154, 388, 476, and 213 µmol/g in ASR at pH 6, corresponding to 2.0, 4.0, 9.4, and 4.7% of the biochar mass, respectively. We recovered 83-88% of the removed MC mass by solvent extraction (Table S6) but did not detect any of the reduction intermediates or products (see below) throughout incubations, suggesting all MCs were removed by Rogue_{OX} predominantly or exclusively through sorption.

The $C_{s,\,max}$ and K_L values, representing sorption capacity and affinity of MCs for Rogue_{OX}, respectively, were highest for DNAN. This was expected based on its high K_{OW} and K_{OC} values (Table 1) and the strong π – π interactions resulting from its electron-withdrawing nitro groups. Despite the low solubility of RDX, the non-aromatic structure may have contributed to the considerably lower $C_{s,max}$ compared to DNAN.^{67, 68} Although NQ has high solubility and the lowest molecular weight, the $C_{s,max}$ for NQ was twice that for NTO on a mass basis, suggesting the charge of NTO hindered its sorption. Overall, Rogue showed significant sorption capacities for MCs, especially for neutral and aromatic MCs such as DNAN. When NQ sorption to SRB and Rogue was compared (Section S5, Figure S7(b)), $C_{s,max}$ for SRB was 98 μ mol/g (1.0% of SRB mass), or one-fourth of the $C_{s,max}$ for Rogue. This shows that Rogue exhibits a greater sorption capacity for MCs than SRB, presumably due to its higher BET surface area (Table S2).

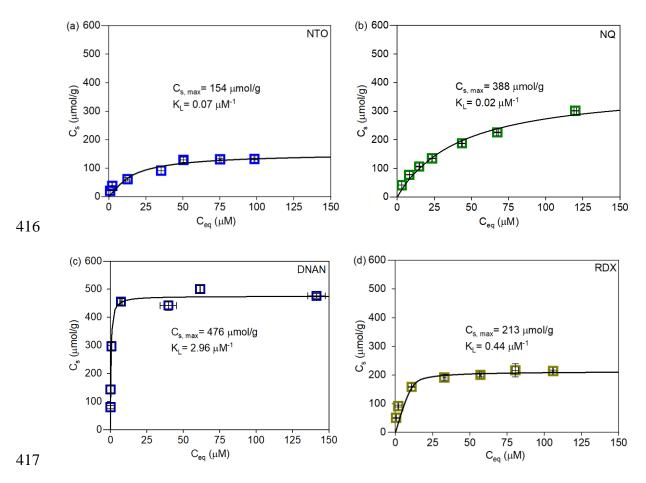


Figure 5. MC sorption to Rogue_{OX} in ASR at pH 6 and the fitted Langmuir isotherms. (a) NTO (b) NQ (c) DNAN (d) RDX

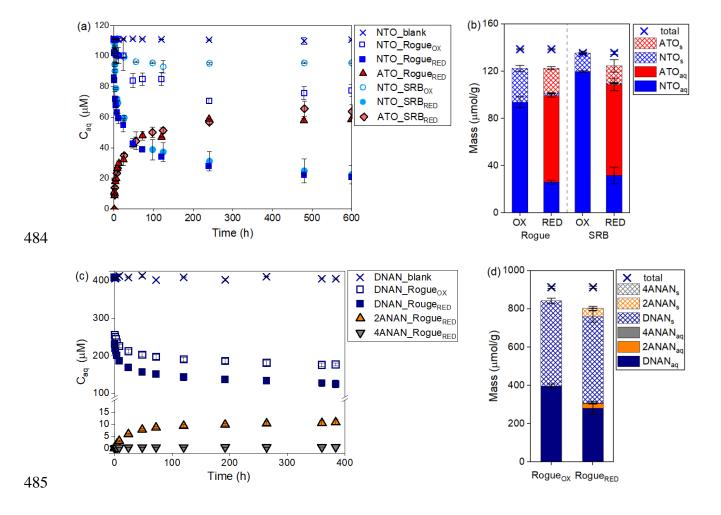
MC reduction by biochar. The reactivity of biochar toward DNAN, RDX, and NQ was assessed by comparing MC removal by Rogue_{OX} (sorption only) and Rogue_{RED} (sorption and reduction). NQ was removed from solution at similar rates and to the same extent with SRB_{OX} and SRB_{RED} (Figure S8), suggesting NQ was removed through sorption to both oxidized and reduced SRB and was not reduced by SRB_{RED}. The similar removal also suggests that the nature and density of sorption sites for NQ were not measurably altered by dithionite reduction. NQ has been reported to undergo reduction with bimetallic particles⁶⁹, but it does not appear to react with reduced black carbon. Consistent with this result, a recent study showed that NQ was inert toward

429	carbonaceous reductants such as dithionite-reduced hydroquinones and humic acids. ⁷⁰ Hence,
430	abiotic reduction by carbonaceous reductants may not be an important fate mechanism for NQ
431	even under highly reducing conditions.
432	In contrast to NQ, NTO, DNAN, and RDX were all reducible by reduced biochar. As
433	shown in Figure 6(a), reduction of NTO by SRB _{RED} in ASR at pH 6 was in good agreement with
434	that in MES buffer (Figure 1(a)), suggesting that the solution matrix did not influence the
435	reactivity of the biochar. Under the same conditions, NTO was similarly reduced to ATO by
436	Rogue _{RED} , indicating the reactivity of reduced biochar toward NTO is not specific to SRB.
437	Interestingly, Rogue _{RED} and SRB _{RED} converted comparable amounts of NTO to ATO (91 and 94
438	$\mu mol/g$, respectively, Table 2). This suggests that the fraction of Rogue ESC reactive toward
439	NTO was about 564 μ mol/g, approximately the same as that for SRB (546 μ mol/g), despite the
440	higher ESC of Rogue. Note that the amount of NTO reduced per gram of SRB or Rogue depends
441	on not the total ESC, but the fraction of ESC that has sufficiently low E_{H} (i.e., contains
442	sufficiently reducing electrons) to degrade NTO. Without knowing the redox potential
443	distributions (i.e., the E _H profiles) of SRB and Rogue, it is not possible to compare the biochars'
444	capacities to degrade NTO.
445	Rogue _{OX} removed 518 μ mol/g of DNAN and 232 μ mol/g of RDX at the end of experiment
446	(Table 2), consistent with the fitted $C_{s,max}$ values of 476 and 213 $\mu mol/g$, respectively (Table 1).
447	In comparison, Rogue_{RED} removed additional 112 μ mol/g of DNAN and 100 μ mol/g of RDX,
448	suggesting these MCs were not only sorbed but chemically reduced by Rogue _{RED} . This was
449	confirmed through identification of reduced products of DNAN and RDX. Unlike NTO,
450	however, DNAN and RDX sorbed more strongly to Rogue, and the sorbed molecules might not

451	be readily available for reduction. Therefore, only relatively small fractions of the DNAN and
452	RDX removed from water was recovered as reduced products.
453	Abiotic reduction of DNAN by Rogue _{RED} was confirmed by the detection of 66 µmol/g of
454	2ANAN and a trace quantity (<2 μmol/g) of 4ANAN in the aqueous and solid phases combined.
455	2ANAN is also the major intermediate product of DNAN during chemical ^{63, 71} and microbial ⁷²
456	reduction, because the ability of the methoxy group to be hydrated by water molecules helps to
457	better solvate the <i>ortho</i> nitro group and enable it to bear a greater negative charge than the <i>para</i>
458	nitro group following one electron reduction of DNAN. ⁷³ We did not observe DAAN in either
459	the aqueous phase or the solid phase (via extraction) throughout the experiment. Additional
460	experiments carried out under the same conditions using 2ANAN as the starting reactant further
461	confirmed that no DAAN was produced from 2ANAN (Figure S9(a)). Based on the yields of
462	2ANAN and 4ANAN and that 6 electrons were required to reduce DNAN to 2ANAN or
463	4ANAN, the fraction of Rogue's ESC that was reactive toward DNAN was 402 μ mol/g,
464	approximately 30% lower than that toward NTO, suggesting NTO is more reducible than DNAN
465	at pH 6. ⁶³
466	In RDX reactors, small amounts of $NO_2^-(\emph{ca}.\ 5~\mu\mbox{M})$ and MNX (<1 $\mu\mbox{M})$ were
467	formed with Rogue _{RED} , but not Rogue _{OX} . MNX and NO ₂ ⁻ are known RDX degradation
468	products and, therefore, their detection supports the finding that RDX was degraded by
469	Rogue _{RED} . Specifically, MNX and NO ₂ ⁻ were formed through reduction, since an addition
470	of two electrons is required for MNX formation and reductive denitration of RDX to form
471	NO ₂ ⁻ has been well-documented. ^{51,74} RDX degradation was further confirmed by the
472	accumulation of NO ₂ ⁻ following repeated additions of RDX in reactors containing
473	Rogue _{RED} , as detailed in Section S6 (Figure S10). The accumulation of NO ₂ ⁻ also suggests

that Rogue could not chemically reduce nitrite, as confirmed independently by a separate experiment using NO₂⁻ as the starting reactant (Figure S9(b)). The mass recovery of RDX with Rogue_{RED} was only 64%, considerably lower than the 96% RDX mass recovery obtained with Rogue_{OX} following the same extraction procedures (Table S7). This suggests *ca.* 36% of the initial RDX was likely transformed by Rogue_{RED}. The incomplete mass balance with Rogue_{RED} (Figure 6(f)) also suggests that RDX may have undergone ring cleavage or other reactions.

Overall, our results confirm that (1) DNAN and RDX can be chemically reduced by biochar through its ESC, and that (2) DNAN and RDX can be removed from water by biochar through concurrent sorption and reduction.



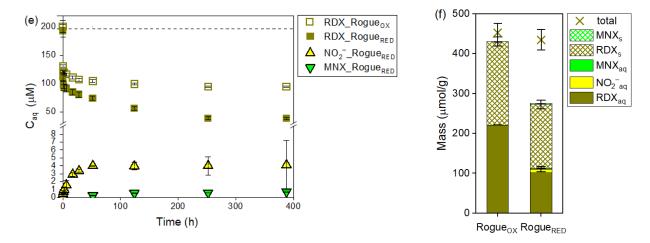


Figure 6. MC reduction by biochar in ASR at pH 6. (a) Aqueous concentration (C_{aq}) of NTO and ATO over time with 0.80 g/L of SRB or Rogue. (b) NTO mass balance. (c) C_{aq} of DNAN and 2ANAN/4ANAN over time with 0.44 g/L of Rogue. (d) DNAN mass balance. (e) C_{aq} of RDX and MNX/NO₂⁻ over time with 0.44 g/L of Rogue. (f) RDX mass balance. "total" is the DNAN or RDX added to blank. Compound names with the subscripts "aq" and "s" represent the masses in the aqueous phase at the end of experiment (*ca.* 400 h) and the extracted masses from the solid phase, respectively.

Table 1. Sorption of MCs by Rogue in ASR at pH 6

MC		NTO	NQ	DNAN	RDX
Structure		O ₂ N N O N O N O N O N O N O N O N O N O N	NH N NO ₂	OCH ₃ NO ₂	NO ₂ N N N N NO ₂
Formulation		IMX-101	IMX-101	IMX-101	IMX-104
		IMX-104		IMX-104	
Physical	M.W. (g/mol)	130.08	104.07	198.13	222.26
Properties ^a	Solubility (mg/L)	16642 ⁵	$2600^{75} - 5000^{69}$	276 ⁵	60^{5}
	Log K _{OW}	$0.37 - 1.03^5$	0.10^{75}	1.64 ⁵	$0.81 - 0.87^5$
	Log K _{OC}	3.03^{5}	_	3.11 ⁵	$0.88-2.40^5$
Isotherm	$C_{s, max} (\mu mol/g)$	154	388	476	213
Parameters ^b	$C_{s,\;max}\left(\%,w/w\right)$	2.0	4.0	9.4	4.7
	$K_L(\mu M^{\text{-}1})$	0.07	0.02	2.96	0.44
	\mathbb{R}^2	0.94	0.96	0.97	0.98

⁴⁹⁶ a M.W.: molecular weight, K_{OW}, K_{OC}: octanol-water and organic carbon-water partition coefficients, respectively. Solubility at 25 °C.

^b Parameters of the isotherms are obtained through Langmuir isotherm fitting, as shown in Figure 5.

Table 2. Summary of MC reduction by biochar at pH 6

MC		NTO	NTO	NTO	DNAN	RDX
Biochar		SRB	SRB	Rogue	Rogue	Rogue
Background solution		50 mM MES	ASR	ASR	ASR	ASR
Removal by RED ^a		112±8	103±8	112±2	630±20	332±19
Removal by OX ^b		24±0	15±2	44±6	518±5	232±20
Δ Removal ^c	(g/lomµ)	88±8	88±6	68±6	112±16	100±6
Product(s) formed	n.	100±7 ^d	91±6 ^d	94±2 ^d	67±7 ^e	14±6 ^f
e ⁻ transferred ^g		600±40	546±40	564±14	402±40	_

499 a RED: reduced biochar (SRB_{RED} or Rogue_{RED})

500 bOX: oxidized biochar (SRB_{OX} or Rogue_{OX})

^c Δ Removal: additional MC removal by reduced biochar than oxidized biochar (Removal by RED – Removal by OX)

502 d ATO formed

498

^e 2ANAN and 4ANAN formed

504 f MNX and NO₂ formed

505 g e⁻ transferred (µmol e⁻/g) =Product(s) formed (µmol/g) × 6 (mol e⁻/mol product)

Conclusion

To the best of our knowledge, this is the first study to demonstrate the ability and capacity of biochar to reductively degrade organic pollutants through its ESC. This degradative capacity can be regenerated *in situ* through chemical or microbial reduction³¹ and utilized repeatedly for pollution mitigation. Electrons stored in wood-derived biochar could reduce NTO to ATO stoichiometrically at pH 6–10. The fraction of biochar ESC reactive toward NTO was significant, *ca*. 500-600 μmol/g, or 26-38% of the ESC measured with ferricyanide, and 12-15% of that measured with DO. In addition to NTO, biochar was able to reduce DNAN and RDX as well as adsorb these MCs. Taken together, these results suggest biochar may serve as both a sorbent and regenerable reactive medium to support simultaneous removal *and* degradation of MCs and potentially other contaminants.

This study supports further investigation and development of biochar-based remediation strategies for military facilities. In particular, the ESC and surface area of biochar may be useful properties for selecting char materials for field applications. This study also offers insights into how pyrogenic black carbons, such as those produced globally from wildfires and deforestation, may represent enormous electron reservoirs and sorbents that influence chemical transformation and transport in the environment. The role of pyrogenic carbons in contaminant geochemistry hence warrants further investigation.

Supporting Information

Sections for of biochar characterization, determination of the pK_a of ATO, ATO sorption, thermodynamic calculations for the redox reactions involved, NQ sorption, and nitrite production from RDX reduction; tables summarizing chemicals used, biochar properties, and experimental

conditions; tables describing MC reduction, sorption, and extraction efficiency; figures					
illustrating biochar ESC reversibility for NTO reduction, batch MC sorption experiments, and					
removal of MC reduction daughter products by biochar.					
Author Contributions					
Conceptualization, P. C. Chiu; investigation, D. Xin and J. Girón; writing-original draft, D.					
Xin; writing-review & editing, all authors, funding acquisition, M. E. Fuller and P. C. Chiu.					
Conflicts of Interest					
There are no conflicts of interest to declare.					
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